

CONSERVATION EQUATIONS

→ Continuity equation

→ Net mass flow rate through cross section's'
$$= \oint \rho \vec{v} \cdot d\vec{s} \quad \text{--- (1)}$$

→ Rate of decrement of mass within the control volume
$$= - \frac{\partial}{\partial t} \iiint \rho dV \quad \text{--- (2)}$$

∴ By conservation of mass we have,

$$\left[\frac{\partial}{\partial t} \iiint \rho dV + \oint \rho \vec{v} \cdot d\vec{s} = 0 \right] \rightarrow \text{integral form}$$

$$\left[\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \vec{v}) = 0 \right] \rightarrow \text{differential form}$$

for unsteady flow.

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→ Momentum equation:

$$\frac{\partial}{\partial t} \oint \rho \vec{v} dV + \oint_S (\rho \vec{v} \cdot d\vec{s}) \vec{v} = - \oint_S P d\vec{s} + \iiint_V \rho \vec{f} dV + F_{viscous}$$

Pressure forces Body forces

↳ Integral form.

$$\frac{\partial}{\partial t} (\rho u) + \nabla(\rho u v) = - \frac{\partial p}{\partial x} + F_{vis} + F_{body}$$

↳ differential form

→ Corollary 1: If the flow is steady and no body forces are acting the reduced form of above equation becomes,

$$\oint_S (\rho \vec{v} d\vec{s}) \vec{v} = - \oint_S P \cdot d\vec{s} + F_{viscous}$$

→ Corollary 2: If the flow is steady, inviscid and no body forces are acting the reduced form of Navier Stokes,

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$$\oint_S (\rho \vec{v} \cdot d\vec{s}) \vec{v} = - \oint_S P d\vec{s}$$

→ Integral form

$$\nabla(\rho u v) = -\partial P / \partial x$$

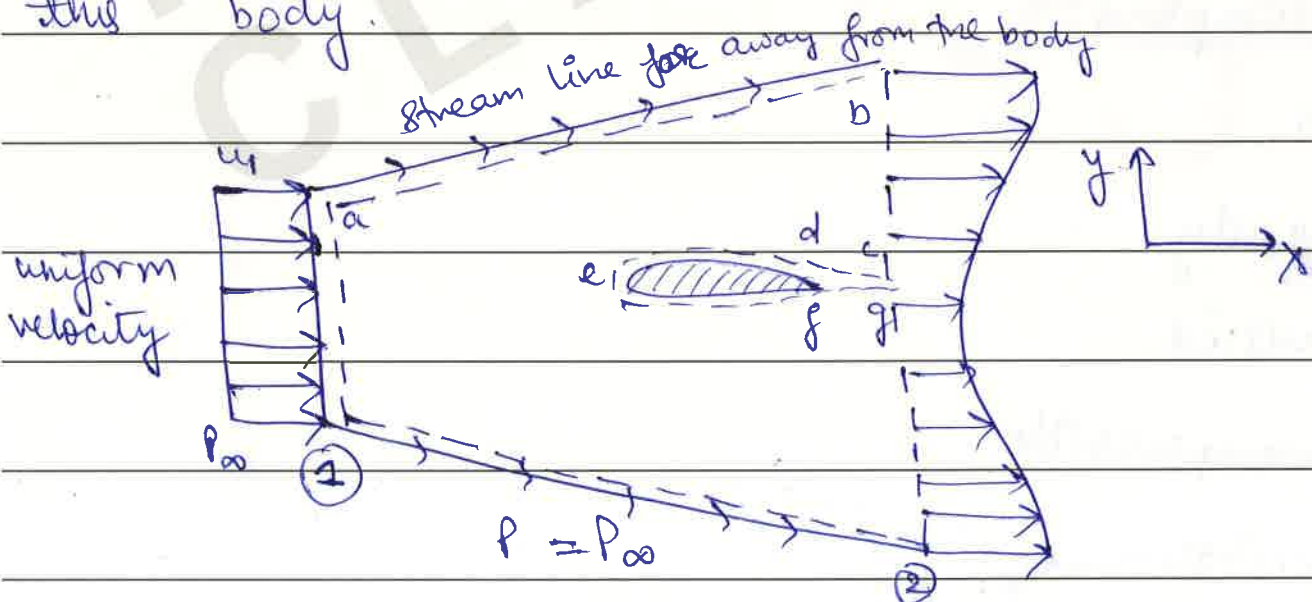
$$\nabla(\rho u v) = -\partial P / \partial y$$

$$\nabla(\rho u v) = -\partial P / \partial z$$

} - differential form

→ Applications of momentum equation (Drag of 2D body)

→ Consider a 2D body in a flow as sketched in figure a control volume is drawn around this body.



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$$D = \int_h^b \rho_2 u_2 (u_1 - u_2) dy$$

steady, no body force, 2D

→ For incompressible flow ' ρ ' is constant and is known,

$$D = \rho \int_h^b u_2 (u_1 - u_2) dy$$

which is applicable for 2D steady incompressible flow with no body force.

→ Ideal potential flow (2D) :

→ Assumptions:

- ① 2D
- ② Steady
- ③ inviscid
- ④ Incompressible
- ⑤ Irrotational

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→ By continuity equation,

$$\frac{\partial}{\partial t} \iiint_V \rho dV + \iint_S \rho \vec{v} \cdot d\vec{s} = 0$$
$$\therefore \boxed{\iint_S \rho \vec{v} \cdot d\vec{s} = 0}$$

→ For incompressible flow, $\rho = c$.

$$\boxed{\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0} \rightarrow \text{continuity equation for steady, incompressible flow}$$

$$\boxed{\nabla \cdot \vec{v} = 0}$$

→ NOTE:

Particles of the flow must rotate about its own mass centre to be called as rotational flow.

→ Rotation:

It is the angle of velocity of particle about its centre of mass.

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Rotation vector $\vec{\omega} = \omega_x \hat{i} + \omega_y \hat{j} + \omega_z \hat{k}$

$$\omega_z = \frac{1}{2} \left(\frac{\partial v}{\partial x} - \frac{\partial u}{\partial y} \right)$$

$$\omega_x = \frac{1}{2} \left[\frac{\partial w}{\partial y} - \frac{\partial v}{\partial z} \right]$$

$$\omega_y = \frac{1}{2} \left[\frac{\partial u}{\partial z} - \frac{\partial w}{\partial x} \right]$$

$$\rightarrow \text{Vorticity} = \vec{\zeta} = \nabla \times \vec{V} = \begin{vmatrix} \hat{i} & \hat{j} & \hat{k} \\ \frac{\partial}{\partial x} & \frac{\partial}{\partial y} & \frac{\partial}{\partial z} \\ u & v & w \end{vmatrix}$$

$$\begin{aligned} \vec{\zeta} &= \hat{i} \left(\frac{\partial w}{\partial y} - \frac{\partial v}{\partial z} \right) - \hat{j} \left(\frac{\partial w}{\partial x} - \frac{\partial u}{\partial z} \right) + \hat{k} \left(\frac{\partial v}{\partial x} - \frac{\partial u}{\partial y} \right) \\ &= \hat{i} (2\omega_x) - \hat{j} (-2\omega_y) + \hat{k} (2\omega_z) \\ &= 2 (\omega_x \hat{i} + \omega_y \hat{j} + \omega_z \hat{k}) \end{aligned}$$

$$\boxed{\nabla \times \vec{V} = \vec{\zeta} = 2\vec{\omega}}$$

vorticity = 2 × rotation

→ Note: If curl of velocity vector $\vec{\zeta} = 0$, the flow is said to be irrotational.